Atty. Docket No.: P65124US0

IN THE CLAIMS:

Please amend/retain/add the claims as follows:

- 1. (Currently Amended) A method for treating a liquid effluent of <u>animal manure</u> pig slurry loaded with <u>significant</u> quantities of nitrogen and phosphorus, comprising the steps of:
- a) adding a basic reagent to <u>a said</u> liquid effluent of pig slurry containing <u>significant quantities</u> <u>more than 500 ppm</u> of nitrogen <u>as ammonia</u> and phosphorus to obtain a pH in <u>a the</u> range from 8.5 to 13; and
- b) diffusing the basified liquid effluent of said pig slurry derived from stage a) in a stream of air having a flow rate of from about 6,000 to 15,000 m³/hr; and
- c) removing up to 80% of the ammoniacal nitrogen from said pig slurry.
- 2. (Previously Presented) The method according to Claim 1, wherein the basic reagent added to stage a) is unslaked or slaked lime in the form of powder, paste or liquid.
- 3. (Previously Presented) The method according to Claim 2, wherein a concentration of lime $Ca(OH)_2$ is a maximum of 1,000 g/litre of reagent.

Atty. Docket No.: P65124US0

- 4. (Previously Presented) The method according to Claim 3, wherein the stage b) is repeated a number of times for the same basified effluent.
- 5. (Previously Presented) The method according to Claim 4, wherein the number of repetitions is in the range from 1 to 50.
- 6. (Previously Presented) The method according to Claim 1, wherein at a start of stage b) an anti-foam catalyst is added, the quantity of which varies from 0 to 1 1/m³ of liquid effluent which is to be treated.
- 7. (Currently Amended) The method according to Claim 1, further comprising $\frac{1}{2}$ in stage c) a step of sifting the liquid effluent derived from stage b).
- 8. (Currently Amended) A device for treating a liquid effluent of pig slurry animal manure loaded with significant quantities of nitrogen and phosphorus by adding a basic reagent to said liquid effluent to obtain a pH in the range from 8.5 to 13 an and diffusing the basified liquid effluent derived in a stream of air, the device comprising:

Attv. Docket No.: P65124US0

a mixing reactor for bringing <u>a</u> the liquid effluent of pig slurry loaded with significant quantities containing more than 500 ppm of nitrogen <u>as ammonia</u> and phosphorus into contact with the basic reagent, said mixing reactor provided with an intake for said effluent and another intake for the basic reagent;

an ammonia-extracting reactor connected to the mixing reactor for extracting up to 80% of the ammoniacal nitrogen from said pig slurry; and

a tank for storing the treated liquid effluent derived from the ammonia-extracting reactor.

- 9. (Previously Presented) The device according to Claim 8, wherein the mixing reactor includes a device for measuring the pH of the medium connected to a means situated on the intake for the basic reagent for regulating automatically the added quantity thereof.
- 10. (Previously Presented) The device according to Claim 9, wherein the ammonia-extracting reactor or degassing reactor comprises a lower part collecting in particular the basified liquid effluent and an upper part in which there is situated a

Atty. Docket No.: P65124US0

diffusion rack provided with nozzles, connected at the lower part to said reactor and including a feed pump, openings being arranged between the two parts to allow exterior air to enter, and an exhaust air fan being connected to said upper part.

- 11. (Previously Presented) The device according to Claim 10, wherein the diffusion rack includes nozzles of the cyclone type.
- 12. (Previously Presented) The device according to Claim
 10, wherein the upper part of the degassing reactor is connected
 to a moisture-reducing unit.
- 13. (Previously Presented) The device according to Claim
 12, further comprising a washing tower connected to the moisturereducing unit allowing the ammonia to be collected or eliminated.
- method removes approximately 40% of said ammoniacal nitrogen from said pig slurry with a slurry flow rate of approximately 3-10 m³ per hour.

Atty. Docket No.: P65124US0

- 15. (New) The method according to Claim 1, wherein said method removes approximately 60% of said ammoniacal nitrogen from said pig slurry with a slurry flow rate of approximately 2-8 m³ per hour.
- 16. (New) The method according to Claim 1, wherein said method removes approximately 80% of said ammoniacal nitrogen from said pig slurry with a slurry flow rate of approximately 1-4 m³ per hour.
- 17. (New) The method according to Claim 1, wherein said pig slurry contains approximately 1800 ppm of nitrogen as ammonia.
- 18. (New) The method according to Claim 17, wherein said method removes approximately 40% of said ammoniacal nitrogen from said pig slurry with a slurry flow rate of approximately $3-10~\text{m}^3$ per hour.
- 19. (New) The method according to Claim 17, wherein said method removes approximately 60% of said ammoniacal nitrogen from said pig slurry with a slurry flow rate of approximately 2-8 m³ per hour.

Atty. Docket No.: P65124US0

20. (New) The method according to Claim 17, wherein said method removes approximately 80% of said ammoniacal nitrogen from said pig slurry with a slurry flow rate of approximately 1-4 $\rm m^3$ per hour.